



First Acidic Macro-Mesocellular Aluminosilicate Monolithic foams "SiAl(HIPE)" and their Catalytic Properties

Damien P. Debecker, Cédric Boissière, Guillaume Laurent, Stéphanie Huet, Philippe Eliaers, Clément Sanchez, Rénal Backov

► To cite this version:

Damien P. Debecker, Cédric Boissière, Guillaume Laurent, Stéphanie Huet, Philippe Eliaers, et al.. First Acidic Macro-Mesocellular Aluminosilicate Monolithic foams "SiAl(HIPE)" and their Catalytic Properties. Chemical Communications, 2015, 51 (74), pp.14018-14021. 10.1039/C5CC05328E . hal-01191422v1

HAL Id: hal-01191422

<https://hal.sorbonne-universite.fr/hal-01191422v1>

Submitted on 7 Sep 2015 (v1), last revised 1 Mar 2016 (v2)

HAL is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers.

L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.

Copyright

First Acidic Macro-Mesocellular Aluminosilicate Monolithic foams "SiAl(HIPE)" and their Catalytic Properties

Damien P. Debecker^{a,*}, Cédric Boissière^{b,*}, Guillaume Laurent^b, Stéphanie Huet^c, Philippe Eliaers^d, Clément Sanchez^b, Rénal Backov^c

A new type of acidic macrocellular and mesoporous silica-alumina foam is obtained via a one pot alkaline sol-gel route coupled with a concentrated emulsion-based templating technique. The mixed oxide monolith exhibits high surface acidity, translating in excellent performance in the acid-catalyzed dehydration of bioethanol to ethene.

Aluminosilicates are of utmost importance as catalysts and catalyst supports.¹ Amorphous aluminosilicates are used as mild acidic supports for various active species like for instance Mo, W or Re oxides for olefin metathesis,² Ni, W, Co and Mo oxides for hydrodesulfurization reaction,³ Ni for reduction reactions,⁴ Pd and Pt for hydrogenation reactions⁵, etc. They are also employed as catalyst themselves in several petrochemical processes, including cracking.⁶ Their acidity can be somewhat tuned to meet the specific requirement of a particular reaction.

Zeolites are synthetic microporous crystalline aluminosilicates, in which Al atoms replace Si atoms in the framework, thereby generating uncompensated charge and strong acidity.^{1a} Even if their composition, acidity and structure can be finely tuned, zeolites usually exhibit only small pores in which the diffusion of reactants and products is hampered. Significant steps forward have been made in the design of truly mesoporous acidic aluminosilicates when templating agents have been used to generate mesopores in zeolitic materials.⁷ Further developments in this field are still thriving, taking benefits of advanced polymer science or original processing techniques.⁸

Nevertheless, whether amorphous or crystalline, micro- or mesoporous, catalytic materials in the form of powders have to be shaped as extrudates, pellets or monoliths before being used in industrial flow processes.⁹ This step is usually not straightforward, as (i) appropriate additives must be found that ensure physical strength without compromising catalytic performance, (ii) diffusion limitations issues must be addressed and (iii) attrition must be avoided.¹⁰ An alternative to shaping powders is to impregnate structured supports with active components.¹¹ There also, potential technical issues are numerous: lack of adherence of the catalytic powder to the walls of the structured support, pore plugging, drastic decrease of the specific loading and so forth.

One-step preparation of structured materials with desired properties is hence highly desirable. In this context, the integration of sol-gel chemistry and physical chemistry of complex fluids has led to the genesis of various advanced functional materials.¹² The one-step preparation of macrocellular silica monoliths is a noteworthy example.¹³ Taking advantage of sol-gel chemistry coupled with an emulsion technique, macroscopic silica blocs of defined shape can be obtained, featuring high surface area and good mechanical

strength (5-7 Mpa Young modulus).¹⁴ The preparation is based on the 'High Internal Phase Emulsion' (HIPE) method.¹⁵ Si(HIPE) can be prepared as self-standing macroscopic objects that can be easily manipulated. Along with other diverse applications, these materials when hybridized¹⁵ proved successful as catalyst supports for lipases used in oleochemistry,¹⁶ for Pd nanoparticles used in C-C coupling,¹⁷ etc. Such materials can be casted directly in tubular reactors and be employed as catalyst supports for flow reactions even with bulky molecules.¹⁸

The incorporation of alumina in such system would pave the way to structured acid catalysts. However, this is not straightforward since chemical synthesis conditions used for the preparation of such materials is systematically based on colloidal or acidic silica chemistry. The latter routes are totally inefficient for the true incorporation of aluminum cationic species in the silica network.¹⁹ While Al in tetrahedral coordination is required to get strongly acid heterogeneous catalysts,²⁰ classical routes usually generate aluminum oxide chunks in octahedral environment.

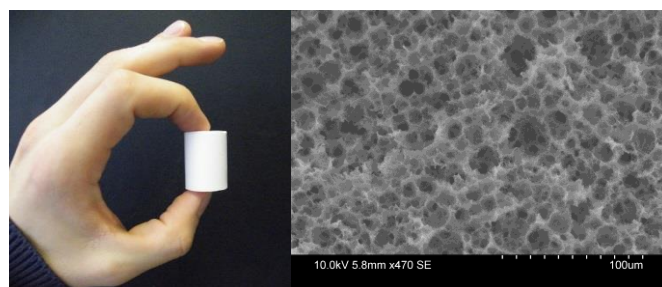


Figure 1. (left) picture of a SiAl(HIPE) monolith, (right) SEM micrograph of the SiAl(HIPE).

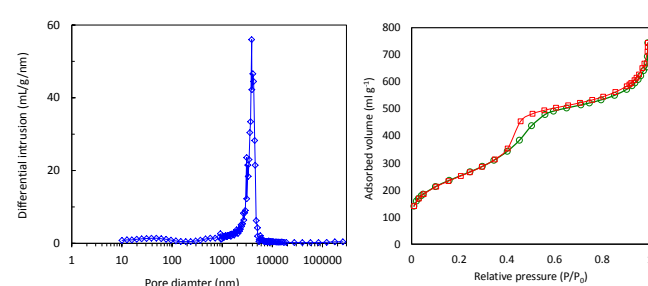


Figure 2. (Left) Size distribution of the macroscopic pore opening obtained by mercury intrusion porosimetry and (right) N₂-sorption isotherms.

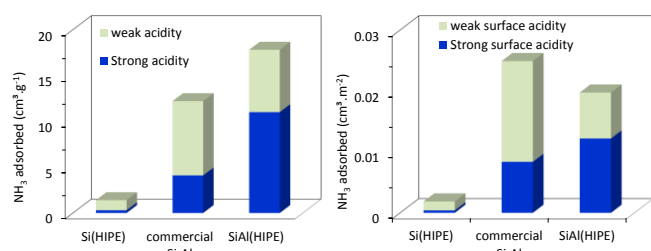


Figure 3. Acidity of SiAl(HIPE) measured by NH₃-chemisorption²¹ and compared to the commercial reference and to Si(HIPE). The acidity is expressed as the amount of NH₃ chemisorbed per gram of catalyst (left) or per m² of catalyst (right).

In the present study the emulsion-based sol-gel route is modified in an alkaline version to meet the ambitious agenda of obtaining, in one step, structured monolithic acidic catalyst bearing hierarchical porosity. The adapted protocol is described in details in the ESI. Briefly, TEOS is incorporated into the emulsion oil phase (dodecane) along with TTAB surfactant. Aluminum isopropoxide is added in the water phase along with TPAOH. A stable emulsion is formed after vigorous stirring and it is simply put to rest for 1 week, washed and calcined. In this way, SiAl(HIPE) was prepared in the form of cm-scale solid monoliths (Fig. 1 and ESI). Macroscopically, SiAl(HIPE) materials appear similar to Si(HIPE).

Pieces of monolith were scratched and observed in scanning electron microscopy (SEM). This reveals the macrocellular structure of the materials (Fig. 1). Interconnected macro-cells have a diameter in the 5-45 μm range. As compared to the well-described Si(HIPE) materials, these macrocells are smaller and present a narrower pore size distribution. This can tentatively be associated with the fact that the SiAl(HIPE) monoliths have been obtained in alkaline pH. In these conditions, condensation reactions are expected to proceed at a faster rate, generating high shearing forces earlier in the emulsion process, thus minimizing the oil droplet diameters and favoring size monodispersity.¹⁴ The atomic Si/Al ratio was estimated over several wide zones of different monolith pieces by the EDX probe mounted on the SEM apparatus to be 9.7 ± 0.2 , not very far from the nominal value of 12. Possibly, a portion of the TEOS did not react at the oil/water interface and was eliminated during the washing. The composition was shown to be fairly homogeneous throughout the sample (ESI). The sample is macroporous as attested by SEM and confirmed by Hg-porosimetry (Fig. 2). SiAl(HIPE) is characterized by an intrusion volume of $10.2 \text{ cm}^3.\text{g}^{-1}$ and a porosity of 89%. Its bulk density is 0.087 g.cm^{-3} . In terms of macrostructure, the alkaline synthesis method allows producing materials as good as the previously reported Si(HIPE). Only the skeletal density tops up at 0.80 g.cm^{-3} , lower than Si(HIPE) ($\sim 1.50 \text{ g.cm}^{-3}$). Macrocells are interconnected by relatively monodisperse pore openings around $4 \mu\text{m}$ in size.

N₂-physisorption measurements demonstrate that SiAl(HIPE) is mesoporous. BET surface area reaches $900 \text{ m}^2.\text{g}^{-1}$. Contrary to the Si(HIPE) series, a t-plot analysis of the isotherm proves that no significant microporosity is present in this materials, the nitrogen uptake at very low relative pressure being due to the high surface area of the samples. A well-defined hysteresis loop in the isotherms translates into a sharp pore size distribution obtained from the adsorption branch, centered at ca. 3.6 nm via the BJH method, and

4.0 nm via Broekhoff and De Boer method (ESI). The presence of a catastrophic desorption at 0.42 in P/P_0 makes impossible the estimation of mesoporous restrictions size distribution.

The samples acidity was measured by NH₃ chemisorption and compared to both a popular commercial aluminosilicate support (Aldrich, Grade 135, $475 \text{ m}^2.\text{g}^{-1}$, 12 wt.% Al₂O₃)²² and Si(HIPE)^{17b} (Fig. 3). The method allows a quantitative analysis of acid sites, with a distinction between weak and strong sites.²¹ As expected, Si(HIPE) is virtually not acidic. Aluminosilicates samples on the other hand retain NH₃ in substantial quantities and SiAl(HIPE) exhibited a total number of acid sites per gram of sample significantly higher than the reference commercial aluminosilicate. The amount of strong acidic sites is almost 3-fold as compared to that of the reference. If the two aluminosilicate materials are compared on a surface basis, the reference exhibits more acidic sites. However SiAl(HIPE) still exhibits more strong acid sites per surface unit.

NMR experiments were conducted to gain insights on the environment of Si and Al atoms in SiAl(HIPE). It appears important, indeed, to verify that the sol-gel process performed in basic pH did not lead to the stabilization of alumina domains dispersed in a silica matrix, but that a truly mixed oxide is formed instead.²⁹ ²⁹Si MAS NMR spectra (Fig. 4) show broader peaks strongly shifted to the left, which is typical for aluminosilicates.²³ This shows that Si and Al precursors have reacted together during the preparation to form Si-O-Al bonds.²⁷ ²⁷Al MAS-NMR spectrum obtained on SiAl(HIPE) shows a large proportion of tetrahedrally coordinated framework Al atoms (signal at ca. 56 ppm, abbreviated Al^{IV}). The latter is typically formed in amorphous aluminosilicates, along with pentacoordinated Al (broad signal around 30 ppm, abbreviated Al^V) and octahedral Al (ca. 2 ppm, abbreviated Al^{VI}).^{2a, 24} In SiAl(HIPE) however, the proportion of Al^{IV} species versus Al^V and Al^{VI} is significantly higher than what is typically found in the reference aluminosilicate.²⁵

Such high content of TET species is characteristic of pre-zeolitic amorphous aluminosilicate materials prepared in basic media in similar conditions.¹⁹ As a consequence, one may explain both the sol-gel condensation and the good incorporation of aluminum centers within silica network by the progressive dodecane/water interfacial hydrolysis of TEOS and deprotonation of silicic acid that locally induces a pH drop (Fig. 5), allowing the polycondensation of fleeting aluminum hydroxide with silicate species. Both TEOS and TTAB diffusions within dodecane phase, and aluminate diffusion within aqueous phase being slow, a progressive self-assembly of positively charged TTAB structuring agent and negatively charged aluminosilicate oligomers has time to take place, creating the mesostructured (SiAl)HIPE.

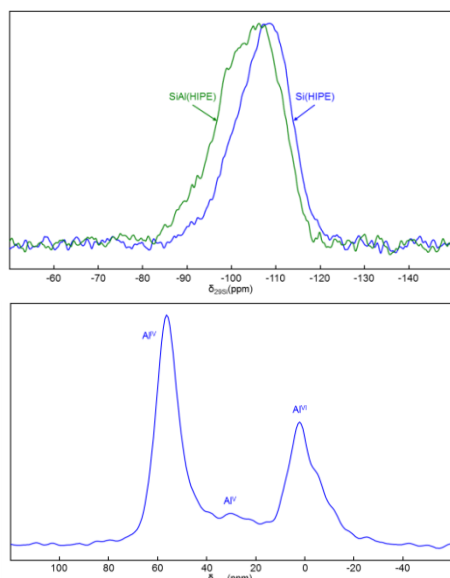


Figure 4. (up) ^{29}Si MAS-NMR spectra for Si(HIPE) and SiAl(HIPE) and (bottom) ^{27}Al MAS-NMR spectrum of SiAl(HIPE).

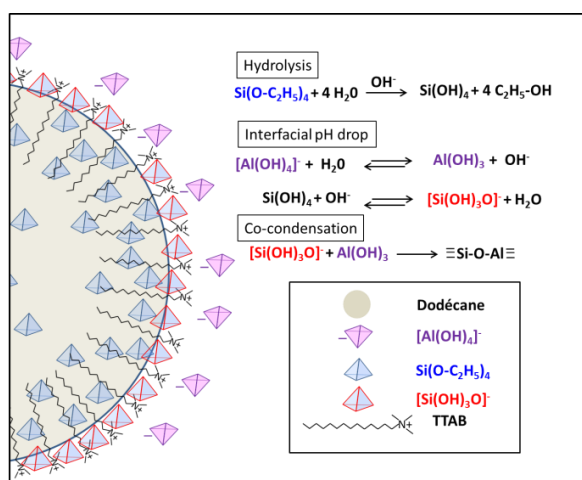


Figure 5. Diffusion-limited Sol-Gel aluminosilicate co-condensation mechanism taking place at the dodecane/water interface.

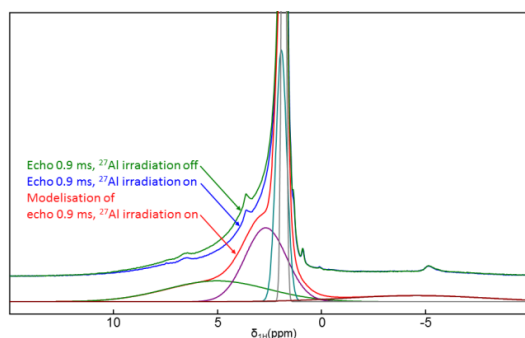


Figure 6. Echo MAS ^1H NMR spectra (sample dehydrated at 200°C). The chemical shift is based on $\{^{27}\text{Al}\}$ - ^1H TRAPDOR experiment (spectra were simulated using dmfit program²⁶; see ESI)

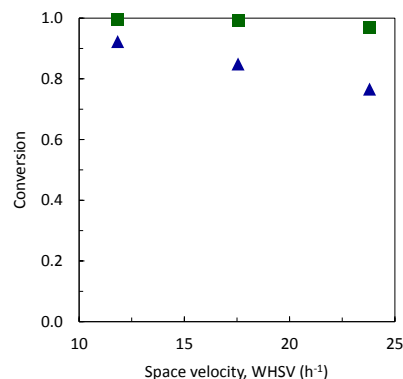


Figure 7. Conversion of ethanol at 400°C with (■) SiAl(HIPE) and (▲) the reference. 1.2 g of catalyst. Selectivity to ethanol is always in the 94.2-97.6 % range (see Table S1 for full product profile). Feed is first generation bioethanol from BioWanze; 99.7wt.% ethanol – 0.3wt.% water evaporated in a preheating zone.

An interesting feature of solid state NMR spectroscopy is the possibility to check spatial proximities between nuclei. For quadrupolar nuclei like ^{27}Al , the TRAPDOR experiment can be used.²⁷ This has been undertaken on a dehydrated sample to discriminate which protons are neighboring ^{27}Al centers and thus which ones are expected to be implicated in catalytic activity. The experiment consists of comparing two spectra, a reference one without ^{27}Al irradiation and an irradiated one, at increasing echo times. The closer the involved spins, the higher will be the dephasing effect. A strong effect is observed around 5 ppm, corresponding to Si-(OH)-Al hydrogen-bonded species; an intermediate effect is seen at 2-2.5 ppm, attributed to Si-OH close to Al center; and no effect is denoted for isolated Si-OH at 1.8 ppm (Fig. 6). Thus, the Si-O-Al network strong Brönsted acidity observed here is matching the high standard of materials assembled from zeolite seeds or amorphous pre-zeolitic materials already reported as powders and produced by precipitation or aerosol processing.¹⁹

From catalytic point of view, both the SiAl(HIPE) and the reference materials catalyze the dehydration of ethanol with high selectivity (~95%) under the conditions used here (Fig. 7). For SiAl(HIPE), conversion remains almost complete up to a space velocity (WHSV) of 23.8 h^{-1} . Note that longer contact times are classically reported in the literature.²⁸ Under our conditions and with a WHSV of 23.8 h^{-1} , the specific productivity reaches 13.3 $\text{g}_{\text{ethene}} \cdot \text{g}_{\text{cat}}^{-1} \cdot \text{h}^{-1}$ for SiAl(HIPE), while the commercial sample produces only 10.4 $\text{g}_{\text{ethene}} \cdot \text{g}_{\text{cat}}^{-1} \cdot \text{h}^{-1}$. As the dehydration of ethanol is known to occur on acid sites such high ethene productivity is to be related with the enhanced acidic properties of the SiAl(HIPE). By-products include butenes, acetaldehyde and diethyl ether. The full product selectivity profile is provided in ESI. Acetaldehyde selectivity systematically remained below 0.5%. While diethyl ether is obtained via a less complete dehydration of ethanol, 1-butene is the product of a consecutive dimerization reaction of ethylene. Thus, as expected, selectivity for diethyl ether was lower and 1-butene selectivity was higher for SiAl(HIPE) as compared to the commercial reference. This again points to a higher acidity and thus higher activity of the SiAl(HIPE).

Combining sol-gel chemistry and physical chemistry of complex fluids, the new route presented here allows preparing meso-macrocellular self-standing objects that are easy to cast and manipulate and that exhibit open and interconnected

macroporosity, high surface area and strong acidic properties. The textural and structural features of these new aluminosilicate monoliths make them particularly attractive for flow processes. The formation of a true mixed aluminosilicate generates abundant and strong surface acid sites, which makes these materials highly attractive for acid-catalyzed reactions. Effectiveness of these catalysts is demonstrated here in the case of bioethanol dehydration, and good performance can be expected in other processes involving bulkier molecules like cracking, isomerization, alkylation reactions, etc.

Acknowledgements.

The French Région Ile de France SESAME program is acknowledged for financial support (700MHz spectrometer).

Notes and references

- (a) A. Corma, *Chem. Rev.*, 1995, 95, 559; (b) G. Busca, *Chem. Rev.*, 2007, 107, 5366.
- (a) D. P. Debecker, M. Stoyanova, U. Rodemerck, P. Eloy, A. Léonard, B.-L. Su and E. M. Gaigneaux, *J. Phys. Chem. C*, 2010, 114, 18664; (b) B. B. Marvey, *Int. J. Mol. Sci.*, 2009, 10, 213; (c) K. Bouchmella, P. Hubert Mutin, M. Stoyanova, C. Poleunis, P. Eloy, U. Rodemerck, E. M. Gaigneaux and D. P. Debecker, *J. Catal.*, 2013, 301, 233.
- (a) E. J. M. Hensen, D. G. Poduval and J. A. R. van Veen, *Ind. Eng. Chem. Res.*, 2007, 46, 4202; (b) T. I. Koranyi and J. B. Nagy, *React. Kinet. Catal. Lett.*, 2005, 85, 131.
- I. H. A. El Maksod, E. Z. Hegazy, S. H. Kenawy and T. S. Saleh, *Adv. Synth. Catal.*, 2010, 352, 1169.
- (a) K. Ezuka, M. Ohshima, H. Kurokawa and H. Miura, *J. Jpn. Pet. Inst.*, 2009, 52, 10; (b) E. Peeters, M. Cattenot, C. Geantet, M. Breyse and J. L. Zotin, *Catal. Today*, 2008, 133, 299.
- (a) A. Ishihara, H. Negura, T. Hashimoto and H. Nasu, *Appl. Catal. A*, 2010, 388, 68; (b) M. A. Ali, T. Tatsumi and T. Masuda, *Appl. Catal. A*, 2002, 233, 77; (c) R. Mokaya and W. Jones, *J. Catal.*, 1997, 172, 211; (d) R. Takahashi, S. Sato, T. Sodesawa and M. Yabuki, *J. Catal.*, 2001, 200, 197.
- C. T. Kresge, M. E. Leonowicz, W. J. Roth, J. C. Vartuli and J. S. Beck, *Nature*, 1992, 359, 710.
- (a) D. P. Debecker, M. Stoyanova, F. Colbeau-Justin, U. Rodemerck, C. Boissière, E. M. Gaigneaux and C. Sanchez, *Angew. Chem. Int. Ed.*, 2012, 51, 2129; (b) X. Zhou, S. Song, A. Duan, Z. Zhao, Y. Gong, X. Wang, J. Li, Y. Wei, G. Jiang and J. Liu, *ChemCatChem*, 2015, DOI: 10.1002/cctc.201500365, In press; (c) F. Colbeau-Justin, C. Boissière, A. Chaumonnot, A. Bonduelle and C. Sanchez, *Advanced Functional Materials*, 2014, 24, 233; (d) M. Fujiwara, A. Sakamoto, K. Shiokawa, A. K. Patra and A. Bhaumik, *Microporous Mesoporous Mater.*, 2011, 142, 381; (e) X. Meng, F. Nawaz and F.-S. Xiao, *Nano Today*, 2009, 4, 292; (f) C. Boissiere, D. Grosso, A. Chaumonnot, L. Nicole and C. Sanchez, *Adv. Mater.*, 2011, 23, 599; (g) X. Xu, T. Zhao, J. Qi, Y. Guo, C. Miao, F. Li and M. Liang, *Mater. Lett.*, 2010, 64, 1660; (h) M. Falco, J. Retuert, A. Hidrobo, C. Covarrubias, P. Araya and U. Sedran, *Appl. Catal. A*, 2009, 366, 269.
- S. Mitchell, N.-L. Michels, K. Kunze and J. Pérez-Ramírez, *Nature Chem.*, 2012, 4, 825.
- (a) V. G. Baldovino-Medrano, M. T. Le, I. Van Driessche, E. Bruneel, C. Alcázar, M. T. Colomer, R. Moreno, A. Florencie, B. Farin and E. M. Gaigneaux, *Catal. Today*, 2015, 246, 81; (b) C. Ngamcharussrivichai, W. Meechan, A. Ketcong, K. Kangwansaichon and S. Butnark, *J. Ind. Eng. Chem.*, 2011, 17, 587.
- (a) T. A. Nijhuis, A. E. W. Beers, T. Vergunst, I. Hoek, F. Kapteijn and J. A. Moulijn, *Catal. Rev. Sci. Eng.*, 2001, 43, 345; (b) F. E. Tuler, E. D. Banús, M. A. Zanuttini, E. E. Miró and V. G. Milt, *Chem. Eng. J.*, 2014, 246, 287; (c) A. Sachse, V. Hulea, A. Finiels, B. Coq, F. Fajula and A. Galarneau, *J. Catal.*, 2012, 287, 62.
- (a) R. Backov, *Soft Matter*, 2006, 2, 452; (b) C. Sanchez, P. Belleville, M. Popall and L. Nicole, *Chem. Soc. Rev.*, 2011, 40, 696.
- A. El Kadib, R. Chimenton, A. Sachse, F. Fajula, A. Galarneau and B. Coq, *Angew. Chem. Int. Ed.*, 2009, 48, 4969.
- F. Carn, A. Colin, M.-F. Achard, H. Deleuze, E. Sellier, M. Birot and R. Backov, *J. Mater. Chem.*, 2004, 14, 1370.
- N. Brun, S. Ungureanu, H. Deleuze and R. Backov, *Chem. Soc. Rev.*, 2011, 40, 771.
- N. Brun, A. B. Garcia, H. Deleuze, M. F. Achard, C. Sanchez, F. Durand, V. Oestreicher and R. Backov, *Chem. Mat.*, 2010, 22, 4555.
- (a) S. Ungureanu, H. Deleuze, O. Babot, M. F. Achard, C. Sanchez, M. I. Popa and R. Backov, *Appl. Catal. A*, 2010, 390, 51; (b) S. Ungureanu, H. Deleuze, C. Sanchez, M. I. Popa and R. Backov, *Chem. Mat.*, 2008, 20, 6494.
- N. Brun, A. Babeau-Garcia, M. F. Achard, C. Sanchez, F. Durand, G. Laurent, M. Birot, H. Deleuze and R. Backov, *Energy Environ. Sci.*, 2011, 4, 2840.
- S. Pega, C. Boissière, D. Grosso, T. Azaïs, A. Chaumonnot and C. Sanchez, *Angew. Chem. Int. Ed.*, 2009, 48, 2784.
- G. Busca, Chapter 6 - Metal Oxides as Acid-Base Catalytic Materials, Elsevier, Amsterdam, 2014.
- D. P. Debecker, D. Hauwaert, M. Stoyanova, A. Barkschat, U. Rodemerck and E. M. Gaigneaux, *Appl. Catal. A*, 2011, 391, 78.
- D. P. Debecker, M. Stoyanova, U. Rodemerck, A. Leonard, B.-L. Su and E. M. Gaigneaux, *Catal. Today*, 2011, 169, 60.
- G. J. Kennedy, J. W. Wiench and M. Pruski, *Solid State Nucl. Magn. Reson.*, 2008, 33, 76.
- E. J. M. Hensen, D. G. Poduval, P. C. M. M. Magusin, A. E. Coumans and J. A. R. van Veen, *J. Catal.*, 2010, 269, 201.
- (a) D. P. Debecker, M. Stoyanova, U. Rodemerck and E. M. Gaigneaux, *J. Mol. Catal. A*, 2011, 340, 65; (b) M. May, M. Asomoza, T. Lopez and R. Gomez, *Chem. Mat.*, 1997, 9, 2395.
- D. Massiot, F. Fayon, M. Capron, I. King, S. Le Calvé, B. Alonso, J.-O. Durand, B. Bujoli, Z. Gan and G. Hoatson, *Magn. Reson. Chem.*, 2002, 40, 70.
- C. P. Grey and A. J. Vega, *J. Am. Chem. Soc.*, 1995, 117, 8232.
- (a) J. Bi, X. Guo, M. Liu and X. Wang, *Catal. Today*, 2010, 149, 143; (b) D. Fan, D.-J. Dai and H.-S. Wu, *Materials*, 2012, 6, 101; (c) M. Zhang and Y. Yu, *Ind. Eng. Chem. Res.*, 2013, 52, 9505.